

Chap. 8 Laminar flow

前面各章中，我們針對流體的特性已有了詳細的介紹。在這一章中我們將針對在大氣中會見到的 **Laminar flow** 做討論。

在前面幾章裡我們已經介紹過了 **Turbulent flow**，而在大氣之中，**Laminar flow** 和 **Turbulent flow** 時常相伴隨產生，但兩者特性卻完全不同。現在我們就以 **Turbulent flow** 做對照，來區分它和 **Laminar flow** 之相異性。

- { **Laminar flow** : fluid moves in layers
- { **Turbulent flow** : irregular motion, macroscopic mixing motion (the fluid mixes violently as moving along)

其實我們從上一章中所介紹的 Reynold number 也可以清楚的分別出 **Turbulent flow** 和 **Laminar flow**。

$$Re = \frac{UL}{\nu} < 3000 \Rightarrow \text{Laminar flow}$$

$$\frac{U^2}{L} : \text{momentum}$$

$$\nu \nabla^2 u : \text{viscous force}$$

若 Re 小 : viscous force constraints the motion of fluid in parallel layers

\Rightarrow **Laminar flow**

註：Re 越大，越有可能形成亂流，但並不是絕對；在不同的環境中，Re 有不同的臨界值。

下面我們再舉幾個例子，試著從數學的觀點來探討有關 **Laminar flow** 的問題。

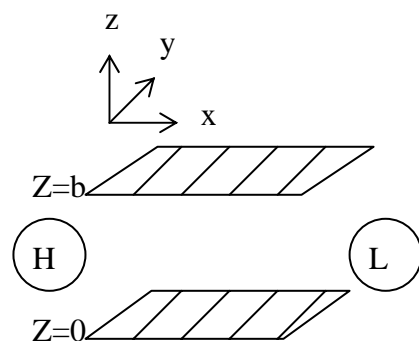
[e.g.] Laminar flow of incompressible flow through straight channels with parallel boundaries

$$u \neq 0, v = 0, w = 0$$

$$\Rightarrow \nabla \cdot \bar{u} = \frac{\partial u}{\partial x} = 0, u = u(t, y, z)$$

$$\rho \frac{d\bar{u}}{dt} = \rho \bar{g} - \nabla p + \mu \nabla^2 \bar{u}$$

x-component :



《圖 8-1》

$$\begin{aligned} & \rho \left(\frac{\partial u}{\partial t} + u \frac{\partial u}{\partial x} + v \frac{\partial u}{\partial y} + w \frac{\partial u}{\partial z} \right) \\ &= \rho g_x - \frac{\partial p}{\partial x} + \mu \left[\left(\frac{\partial^2}{\partial x^2} + \frac{\partial^2}{\partial y^2} + \frac{\partial^2}{\partial z^2} \right) u \right] \\ & \rho \frac{\partial u}{\partial t} = - \frac{\partial p}{\partial x} + \mu \left(\frac{\partial^2}{\partial y^2} + \frac{\partial^2}{\partial z^2} \right) u \\ \Rightarrow & 0 = - \frac{\partial p}{\partial y} \Rightarrow p \text{ is indep. of } y \\ & 0 = \rho g + \frac{\partial p}{\partial z} \quad (\text{静力平衡}) \end{aligned}$$

if the fluid is steady laminar flow :

$$u = u(y, z) \Rightarrow u = u(z) \quad (\text{why?})$$

$$\begin{cases} -\frac{\partial p}{\partial x} + \mu \frac{\partial^2 u}{\partial z^2} = 0, & \frac{\partial p}{\partial x} \text{ is indep. of } z \\ \text{B.C. : 1. at } z=0, u=0 \\ \quad \quad \quad 2. \text{ at } z=b, u=0 \end{cases}$$

$$\int \left[-\frac{\partial p}{\partial x} + \mu \frac{\partial}{\partial z} \left(\frac{\partial u}{\partial z} \right) = 0 \right] dz \Rightarrow -\frac{\partial p}{\partial x} z + \mu \frac{\partial u}{\partial z} = c_1,$$

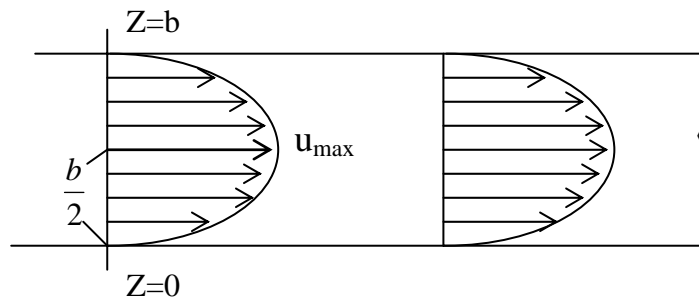
$$\int \left(-\frac{\partial p}{\partial x} z + \mu \frac{\partial u}{\partial z} = c_1 \right) dz \Rightarrow -\frac{1}{2} \frac{\partial p}{\partial x} z^2 + \mu u = c_1 z + c_2$$

$$\Rightarrow u = \frac{1}{2\mu} \frac{\partial p}{\partial x} z^2 + C'_1 z + C'_2 \quad (8-1)$$

$$\Rightarrow \begin{cases} \text{by B.C. 1, } 0 = C'_2 \\ \text{by B.C. 2, } 0 = \frac{1}{2\mu} \frac{\partial p}{\partial x} b^2 + C'_1 b \\ \quad \quad \quad \Rightarrow -\frac{1}{2\mu} \frac{\partial p}{\partial x} b = C'_1 \end{cases}$$

$$\Rightarrow u = \frac{1}{2\mu} \left(-\frac{\partial p}{\partial x} \right) (bz - z^2) = \frac{1}{2\mu} \left(\frac{\partial p}{\partial x} \right) \left[\left(z - \frac{b}{2} \right)^2 - \frac{b^2}{4} \right]$$

$$\Rightarrow z = \frac{b}{2}, u = u_{\max} = \frac{1}{2\mu} \left(-\frac{\partial p}{\partial x} \right) \left[\left(z - \frac{b}{2} \right)^2 - \frac{b^2}{4} \right]$$



《圖 8-2》

現在我們再來看另一個例子。

【e.g.】

如《圖 8-3》；在一流體的底部有一平行板，以 v_0 的速度沿Y軸移動。

$$v \neq 0, \quad \frac{\partial v}{\partial y} = 0 \text{ (沿 } y \text{ 軸各點相同)}$$

$$u = 0, \quad v = v(z, t), \quad w = 0$$

$$\Rightarrow \rho \frac{\partial v}{\partial t} = \mu \frac{\partial^2 v}{\partial z^2}$$

$$\Rightarrow \frac{\partial v}{\partial t} = \nu \frac{\partial^2 v}{\partial z^2} \quad (8-2)$$

$$\left\{ \begin{array}{l} \text{I.C. } V = 0 \text{ for all } z, \text{ at } t \leq 0 \\ \text{B.C. } \begin{array}{l} 1. \text{ at } z = 0, v = v_0, t > 0 \\ 2. \text{ at } z = \infty, v = 0, t > 0 \end{array} \end{array} \right.$$

There are at least three ways to solve this equation :

1. Separation of variables
2. Method of Laplace transform
3. Similarity solution

We use similarity solution to solve the equation :

$$z, t, \nu \Rightarrow \begin{cases} 3 \text{ variables} \\ 2 \text{ dimensions} \end{cases}$$

$$\Rightarrow 3 - 2 = 1, \Rightarrow \text{non-dimensional parameter}$$

$$\pi = z^{a_{11}} t^{a_{12}} \nu^{a_{13}} \Rightarrow a_{11} : a_{12} : a_{13} = 1 : -1/2 : -1/2$$

$$\Rightarrow \pi = \frac{z}{\sqrt{\nu t}}$$

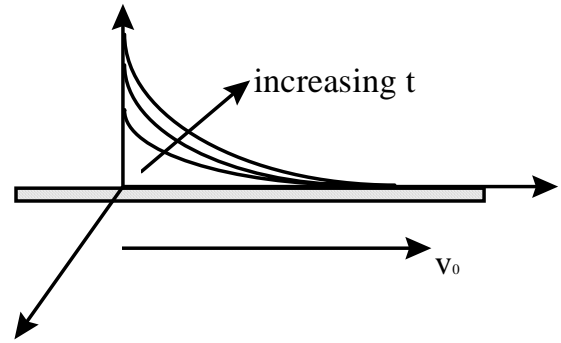
$$\text{令 } \eta = \frac{z}{\sqrt{4\nu t}}, \text{ 設 } v = v_0 f(\eta)$$

$$\frac{\partial v}{\partial t} = v_0 \frac{\partial f(\eta)}{\partial t} = v_0 \frac{\partial f(\eta)}{\partial \eta} \frac{\partial \eta}{\partial t} = v_0 \frac{\partial f(\eta)}{\partial \eta} \left(-\frac{1}{2} \frac{\eta}{t} \right) \rightarrow \frac{1}{\sqrt{4\nu t}}$$

$$\frac{\partial^2 v}{\partial z^2} = v_0 \frac{\partial^2 f(\eta)}{\partial z^2} = v_0 \frac{\partial}{\partial z} \left(\frac{\partial f(\eta)}{\partial z} \right) = v_0 \frac{\partial}{\partial z} \left(\frac{\partial f(\eta)}{\partial \eta} \frac{\partial \eta}{\partial z} \right)$$

$$= \frac{v_0}{\sqrt{4\nu t}} \frac{\partial^2 f(\eta)}{\partial \eta^2} \frac{\partial \eta}{\partial z} = \frac{v_0}{4\nu t} \frac{\partial^2 f(\eta)}{\partial \eta^2} = v_0 \frac{\eta^2}{z^2} \frac{\partial^2 f(\eta)}{\partial \eta^2} \quad (8-3)$$

我們將式(8-3)代回式(8-2)中：



《圖 8-3》

$$\Rightarrow -\frac{1}{2} \frac{\eta}{t} v_0 \frac{df(\eta)}{d\eta} = \nu v_0 \frac{\eta^2}{z^2} \frac{d^2 f(\eta)}{d\eta^2}$$

$$\frac{\partial^2 f(\eta)}{\partial \eta^2} + \left(\frac{z^2}{\nu 2t \eta^2} \right) \left(\eta \frac{df(\eta)}{d\eta} \right) = 0$$

$$\Rightarrow \begin{cases} \frac{d^2 f(\eta)}{d\eta^2} + 2\eta \frac{df(\eta)}{d\eta} = 0 \\ \text{B.C. 1. } \eta=0, V=V_0 \Rightarrow f(\eta)=1 \\ \quad \quad \quad 2. \eta \rightarrow \infty, V \rightarrow 0 \Rightarrow f(\eta) \rightarrow 0 \end{cases}$$

$$\Rightarrow \frac{df(\eta)}{d\eta} = C_1 e^{-\eta^2} \Rightarrow f(\eta) = C_1 \int_0^\eta e^{-\eta^2} d\eta + C_2 \leftarrow \text{by B.C.}$$

$$\text{by B.C.} \begin{cases} 1. \eta=0, f(\eta)=1 \Rightarrow C_2=1 \\ 2. \eta \rightarrow \infty, f(\eta) \rightarrow 0 \Rightarrow C_1 = \frac{-1}{\int_0^\infty e^{-\eta^2} d\eta} = \frac{-2}{\sqrt{\pi}} \end{cases}$$

$$f(\eta) = 1 - \frac{\int_0^\eta e^{-\eta^2} d\eta}{\int_0^\infty e^{-\eta^2} d\eta} = 1 - \frac{2}{\sqrt{\pi}} \int_0^\eta e^{-\eta^2} d\eta = 1 - \text{erf}(\eta) \quad \rightarrow \text{Error function}$$

$$\begin{aligned} v &= v_0 f(\eta) = v_0 \left[1 - \text{erf}(\eta) \right] = v_0 \left[1 - \text{erf} \left(\frac{z}{\sqrt{4\nu t}} \right) \right] \\ &= v_0 \left(1 - \frac{2}{\sqrt{\pi}} \int_0^{\frac{z}{\sqrt{4\nu t}}} e^{-\eta^2} d\eta \right) \end{aligned}$$

現在我們舉一些例子來代入：

$$1. \frac{V}{v_0} = 0.05 \Rightarrow \eta = 1.38$$

$$\Rightarrow z = 2.76 \sqrt{\nu t}$$

$$2. \frac{V}{v_0} = 0.8 \Rightarrow \eta = 0.18$$

$$\Rightarrow z = 0.36 \sqrt{\nu t}$$

由上面這一個例子中，我們能夠了解下列幾點：

1. 隨著時間的增加，流體因邊界之黏滯效應所產生的速度變化範圍也會增加。
2. 若我們想知道在某一時刻高度 Z 之流體速度，我們只需找出 η 值即可導出其關係式!!

想一想，地球自轉，經過漫長時間後，大氣如何運轉？